



SIZING THE ADMIXER™ STATIC MIXER AND SANITARY STATIC BLENDER

INTRODUCTION

This article provides the necessary information for sizing an Admixer™ for liquid / liquid (single phase) mixing. It is designed to be an accurate yet simple method for obtaining the correct static mixer for various liquid applications.

The proceeding calculations will determine the length, diameter, number of elements and pressure drop of the static mixer. These calculations do not apply to gas/liquid or gas/gas dispersions or emulsions, please contact Admix directly regarding any such cases, or refer to Tech Note #105.

Step 1: Tell us the Facts!

Before actual sizing can begin, the initial conditions must be identified. The following chart has been provided for this use:

| SIZING VARIABLE | VALUE | UNITS |
|------------------------------|--------------|--------------|
| Mixing Medium(s) | | |
| (Q) Flow Rate | | GPM |
| (D) Existing Pipe Diameter | | Inches |
| (μ) Absolute Viscosity | | CPS |
| (SG) Specific Gravity | | |
| (ΔP) Max Allowable Head Loss | | PSI |
| (T/P) Temperature / Pressure | | °F/PSI |
| Existing Pipe Material | | |
| Sidestream Injection? | | |
| Special Requirements? | | |

Step 2: Go With The Flow! **(Calculate Reynold's Number)**

Reynold's number must be calculated in order to identify if the pipe flow is turbulent, laminar, or transitional. Reynold's number can be calculated as follows:

$$\text{Reynold's } \# \text{ (Re)} = \frac{3157 \cdot Q \cdot SG}{\mu \cdot D}$$

Q = Flow Rate (GPM)

SG = Specific Gravity

μ = Absolute Viscosity (cps)

D = Pipe Inside Diameter (inches)

Step 3: It's Elementary! **(Select the Number of Elements)**

Using the pipe Reynold's Number (Re) determined above, locate the proper flow regime and Re to select the number of elements required. As explained by the table, it is necessary to add more elements when a wide ratio of fluid viscosities and/or volumes are present. Please remember that these values are guidelines, and should be checked by your local representative or home office.

| Flow Regime | Reynold's Number (Re) | No. of Element | Number of Elements to add if Viscosity ratio between fluids exceeds 1000:1 | Number of Elements to add if Volumetric ratio between fluids exceeds 100:1 |
|--------------------|------------------------------|-----------------------|---|---|
| Laminar | <1 | 24 | 6 | 6 |
| | 1-10 | 18 | 6 | 6 |
| | 11-50 | 14 | 6 | 6 |
| | 51-100 | 12 | 6 | 6 |
| | 101-500 | 10 | 6 | 6 |
| Transitional | 501-1000 | 8 | 4 | 4 |
| | 1001-2000 | 6 | 4 | 4 |
| Turbulent | 2001-5000 | 4 | 2 | 2 |
| | 5001 + | 2 | 2 | 2 |

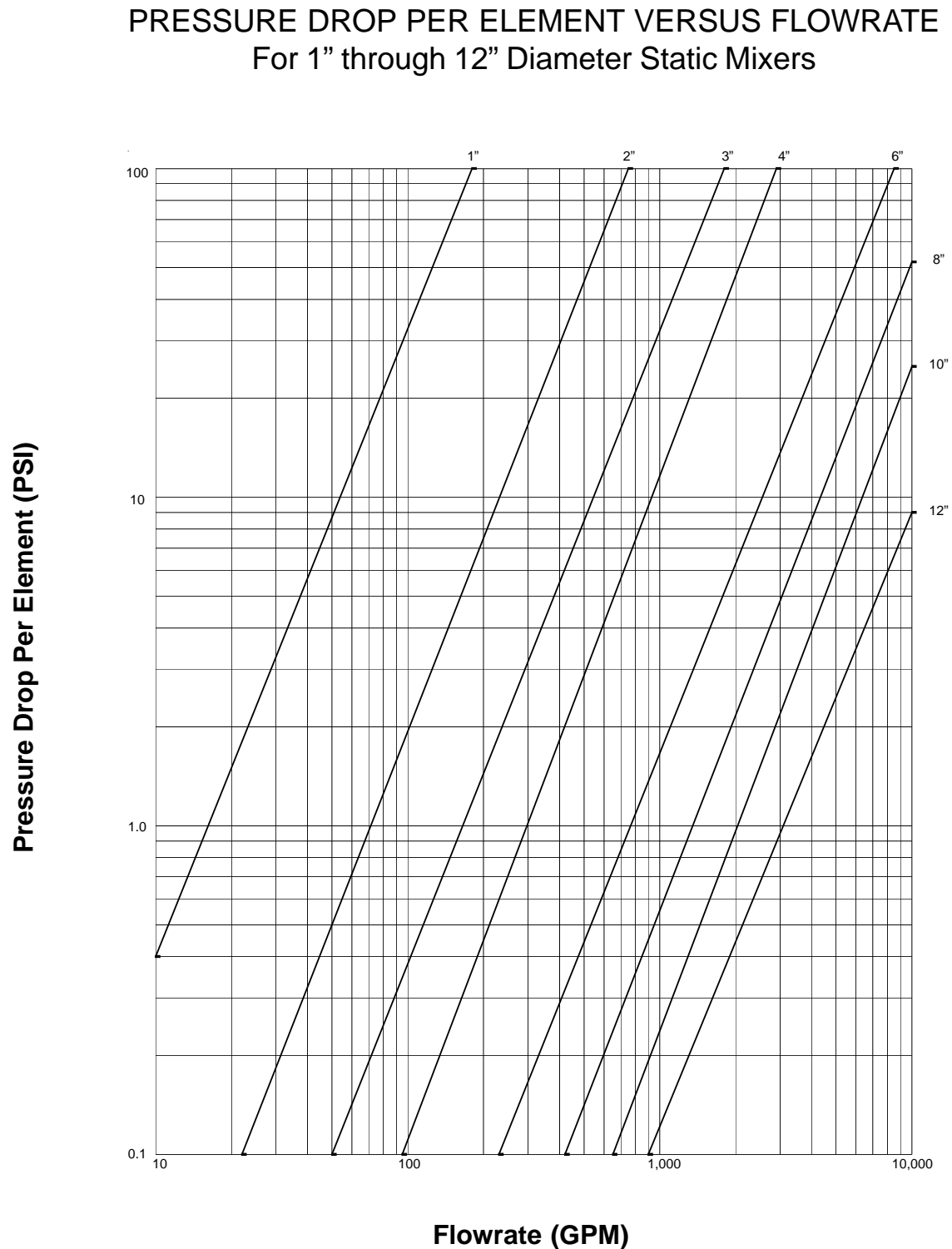
Diameter and Length

For most circumstances, the in-situ piping will determine the mixer diameter. However, it is possible that alternate sizes are needed to accomplish more thorough mixing, reduce pressure drop, or increase dispersion capability. The mixer length will be based on the number of elements required. An approximate length can be determined by multiplying the number of elements by 1.5.

Step 4: Check Your Pressure!
(Calculate Pressure Drop ΔP)

1. To graphically determine pressure drop:

If the process materials are waterlike, with S.G. = 1.0 and viscosity less than 10 cps, the graph below will provide an approximate value of expected pressure drop per element. If the fluids have properties other than that of water, a manual calculation of pressure drop follows.



2. For non waterlike materials where viscosity is greater than 10:

a) Recheck the value for Reynold's number calculated at step #2. Using this value, determine the associated friction factor for the mixer housing using the graph on page 4 (Friction Factors for Clean Commercial Steel and Wrought Iron Pipe).

b) Now calculate P_H of the empty housing without mixing elements.

$$P_H = \frac{0.0135 \cdot f \cdot L \cdot SG \cdot Q^2}{D^5}$$

where f = friction factor
 L = length of pipe (ft)

c) Using the Reynold's number from Step #2, calculate the flow factor, Ff to compensate for the headloss caused by the mixing elements.

| | |
|-----------------------|--------------------------|
| if $Re < 10$, | $Ff = 6.5$ |
| if $10 < Re < 1000$, | $Ff = 1.53 (Re)^{0.45}$ |
| if $Re > 1000$, | $Ff = 8.5 \ln (Re) - 16$ |

d) Does this compute?

The total mixer pressure drop or head loss can now be found by multiplying the housing head loss (P_H) by the element flow factor (Ff)

$$\Delta P \text{ (PSI)} = P_H \times Ff$$

Step 5: Watch your Speed! **(Check Mixer Velocity)**

For turbulent flow applications, it is generally recommended that a minimum velocity of 1.0 Ft/sec be maintained. For best performance, specific applications such as liquid-liquid dispersions may require as high as 7-8 Ft/Sec. For most blending applications, a velocity of 2-3 Ft/Sec. is sufficient.

$$(V) = 0.408 \frac{Q}{D^2}$$

V = Velocity in Ft/Sec

SAMPLE WORKSHEET

Results:

Step 2: Re _____

Step 3: n (# of elements) _____

Dia _____ Length _____

Step 4: f _____

P_H _____

Ff _____

ΔP (PSI) _____

Step 5: V _____

Friction Factor Example

From the chart on page 4, a mixer with a Reynold's Number (Re) of 200,000 within a 4" Sched. 40 pipe will have a friction factor (f) of .0185.

FRICTION FACTORS FOR CLEAN COMMERCIAL STEEL AND WROUGHT IRON PIPE

